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Power management strategy for vehicular-applied hybrid fuel cell/battery power system

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ABSTRACT

In this paper, a control strategy for a hybrid PEM (proton exchange membrane) fuel cell/BES (battery energy system) vehicular power system is presented. The strategy, based on fuzzy logic control, incorporates the slow dynamics of fuel cells and the state of charge (SOC) of the BES. Fuel cell output power was determined according to the driving load requirement and the SOC, using fuzzy dynamic decision-making and fuzzy self-organizing concepts. An analysis of the simulation results was conducted using Matlab/Simulink/Stateflow software in order to verify the effectiveness of the proposed control strategy. It was confirmed that the control scheme can be used to improve the operational efficiency of the hybrid power system.

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1. Introduction

Environmental issues, energy crises, and concerns regarding peaking oil production have spurred research into and development of various types of hybrid electric vehicles. A fuel cell (FC)-powered hybrid vehicle is considered in this paper. Fuel cells offer high power density and low-to-zero emissions. Among the various FC types available, the proton exchange membrane (PEM) FC is the most promising for power systems to be used in automobile, residential, industrial, and other applications. The FC power converter system, for example, consists of a DC/DC converter to boost the stack voltage to a higher level, and a DC/AC inverter to drive the motor. Several variations of power converter architecture have been proposed in the literature [1–6], each entailing advantages and disadvantages.

In view of the fact that fuel cells alone might not be sufficient to satisfy the load demands in vehicular applications, in recent years, several control strategies for hybrid systems incorporating fuel cells and energy storage devices, such as super capacitors or/and batteries, have been presented. Meanwhile, intelligent control theory, for instance fuzzy logic and genetic algorithm, has been introduced to the control process. Because fuzzy control can readily incor-

porate human intelligence in complicated control practice based on human knowledge and experience. It has been demonstrated that a fuzzy controller is very effective to manage power flows in fuel cell powered vehicles hybridizing battery or/and ultracapacitors [6-10]. However, frequent load variations and unexpected driving conditions are inevitably uncertainties. Besides, aging stack and varying subsystems will cause the unsuitable output value obtained from pre-given fuzzy rule tables. In those foregoing reference papers, fuzzy control strategies have been focused on the pre-defined rule tables and an on-line self-organizing of fuzzy output value has not been considered. Hence, a fuzzy control strategy for instantaneous fuel cell power management including on-line self-organizing has been proposed. It is realized by modifying the fuzzy logic based output power of fuel cell. Moreover, to deal with the error in estimating the SOC, SOC diagnosis is introduced into the fuzzy control. That is, the judgment of charge upper limit and that of discharge lower limit are considered and they are introduced into fuzzy rule table indicated by very low (VL) and very high (VH), respectively.

The paper is organized as follows. Section 2 presents the structure of fuel cell powered vehicular power system. The model of the fuel cell system is described in Section 3 to properly represent the slow dynamics of fuel cell associated with the gas flows and the fuel processor operation. Then, the dynamic modeling of battery energy system is presented. Section 4 describes a fuzzy logic based power management strategy. Simulation results and validation analysis are discussed in Sections 5 and 6, respectively. Section 7 is the conclusions.

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Nomenclature

Fuel	coll	system	

Tuci ccii s	system
B_{fc}, C_{fc}	constants to simulate the activation over voltage in
5 5	FC system [A ⁻¹] and [V]
E_{fcs}	Nernst instantaneous voltage [V]
$E_{\alpha\alpha\nu}^{oc\nu}$	standard no load voltage [V]
F	Faraday's constant
Kan	anode valve constant
Kun	hydrogen valve molar constant
K _{H2}	water valve molar constant
KH ₂ 0	modeling constant
M.	molar mass of hydrogen
NH2	number of sories fuel cells in stack
INO N	number of fuel cell stacks in parallel
™ _{fc_p}	humber of fuer cell stacks in paraller
p_{H_2}	nydrogen partial pressure
p_{H_2O}	water partial pressure
p_{O_2}	oxygen partial pressure
q_{O_2}	input molar flow of hydrogen
$q_{\rm H_2}^{in}$	hydrogen input flow
aout	hydrogen output flow
a^r	hydrogen flow that reacts
ч _{Н2}	EC system current
I _{fc}	re system current
Rgas pint	universal gas constant
R_{fc}^{inc}	
T	absolute temperature
U	utilization rate
Van	volume of anode
V _{fcs}	DC output voltage of FC system [V]
η_{act}	activation over voltage [V]
η_{ohmic}	ohmic over voltage [V]
$ au_{ m H_2}$	hydrogen time constant
τ_{0_2}	oxygen time constant
$\tau_{\rm H_2O}$	water time constant
Battery e	nergy system
I _{bat}	battery current (A)
R_{hat}^{int}	internal resistance
R _{ch}	internal resistance of charge
R _{dis}	internal resistance of discharge
SOC	state of charge
<i>SOC</i> _{ini}	initial value of SOC
Vocv	open circuit voltage of battery (V)
η	efficiency
η_{ch}	efficiency of charge
η_{dis}	efficiency of discharge
1415	
Power co	ntrol strategy
P _{hat}	power of BES
P_{fc}	power of fuel cell system
Pload	demand of vehicular power system
P_{c}^{\min}	minimum power output of fuel cell system
JC pmax	maximum power output of fuel cell system
fc	indxiniani power output of fuer cen system
Philin	minimum power output of BES
Phat	maximum power output of BES
P _{fc_net}	net power of fuel cell system
P _{stack}	tuel cell stack power output
P_{BOP}	auxiliary power for BOP
P _{fc_fuzzy}	fuel cell power fuzzy value
SOC _{ref}	reference value of SOC
SOC ^{min}	minimum SOC
SOC ^{max}	maximum SOC
SOC _{diag}	diagnoses status of SOC

V _{c_net}	mean voltage of each cell based on the net power for
	FC system
М	medium
S	small
VS	very small
L	low
VL	very low
Н	high
VH	very high
N	normal
$-\Delta \overline{h}_f$	hydrogen's high heating value (286 kJ mol $^{-1}$)
η_{fcs}	efficiency of fuel cell system
τ_{conv}	time constant of DC/DC converter



Fig. 1. Structure of vehicular power system.

2. Structure of FC-powered vehicular power system

The power system configuration is illustrated in Fig. 1. The FC system consists of two stacks in parallel. It is connected to a DC link via a DC/DC converter, the efficiency of which is assumed to be 90%. Directly connected to the DC link is a battery to supply the transient energy demand and peak loads required during acceleration and deceleration. Under transient conditions, and because the FC current dynamics were intentionally reduced, the battery supplies all other load variations. An electrical traction machine is fed by the DC bus via a DC/AC inverter, the efficiency of which is assumed to be 100%. That is only the power converter loss of the DC/DC converter is considered and that of the DC/AC inverter is assumed to be 90% of fuel cell output power. The vehicular power system as modeled by Matlab/Simulink/Stateflow software is illustrated in Fig. 2.

3. Performance and modeling of fuel cell and battery

3.1. Dynamic modeling of a PEM fuel cell system

The relationship between the molar flow of hydrogen through the valve and its partial pressure inside the channel can be expressed as [11]

$$\frac{q_{\rm H_2}}{p_{\rm H_2}} = \frac{K_{an}}{\sqrt{M_{\rm H_2}}} = K_{\rm H_2} \tag{1}$$

With regard to the hydrogen molar flow, there are three significant factors: hydrogen input flow, hydrogen output flow, and hydrogen flow during a reaction [11]. The relationship among these factors can be expressed as

$$\frac{d}{dt}p_{\rm H_2} = \frac{R_{gas}T}{V_{an}}(q_{\rm H_2}^{in} - q_{\rm H_2}^{out} - q_{\rm H_2}^r)$$
(2)

According to the basic electrochemical relationships between the hydrogen flow and the FC system current, the flow rate of



Fig. 2. Vehicular power system modeled by Matlab/Simulink/StateFlow.

reacted hydrogen is given by

$$q_{\rm H_2}^r = \frac{N_0 I_{fc}}{2F} = 2K_r I_{fc}$$
(3)

Using Eqs. (1) and (3) and applying Laplace's transform, the hydrogen partial pressure can be obtained in the *s* domain, as in [11]

$$p_{\rm H_2} = \frac{1/K_{\rm H_2}}{1 + \tau_{\rm H_2} s} (q_{\rm H_2}^{in} - 2K_r I_{fc}) \tag{4}$$

where

$$\tau_{\rm H_2} = \frac{V_{an}}{K_{\rm H_2} R_{\rm gas} T} \tag{5}$$

Similarly, the water partial pressure and the oxygen partial pressure can be obtained. In the power system discussed in this paper, the two FC stacks, as already mentioned, are connected in parallel. The polarization curve for the PEM FC is obtained from the sum Table 1

PEM fuel cell system model parameters [1-2].

B _{fc}	0.04777 [A ⁻¹]	τ_{0_2}	6.74 [s]
C_{fc} E_0 N_0 $N_{fc,p}$ R_{gas} K_r R^{int}_{fc}	$\begin{array}{c} 0.0136 \ [V] \\ 0.95 \ [V] \\ 350 \\ 2 \\ 8314.47 \ [J \ kmol^{-1} \ K^{-1}] \\ 9.0688 \times 10^{-7} \ [kmol \ s^{-1} \ A^{-1}] \\ 0.177 \ [\Omega] \end{array}$	K_{O_2} K_{H_2O} τ_{H_2} K_{H_2} U $r_{H.O}$ T	2.1 × 10 ⁻⁵ [kmol s ⁻¹ atm ⁻¹] 7.716 × 10 ⁻⁶ [kmol s ⁻¹ atm ⁻¹] 3.37 4.22 × 10 ⁻³ [kmol s ⁻¹ atm ⁻¹] 0.8 1.168 343 [K]

of Nernst's voltage, the activation over voltage and the ohmic over voltage. Assuming a constant temperature and oxygen concentration, the FC output voltage is presented as follows [1–2,5].

$$V_{fcs} = E_{fcs} + \eta_{act} + \eta_{ohmic} \tag{6}$$

where

$$\eta_{act} = -B_{fc} \ln(C_{fc}I_{fc}) \tag{7}$$

$$\eta_{ohmic} = -R_{fc}^{int} I_{fc} \tag{8}$$

The Nerst's instantaneous voltage may be expressed as [5]

$$E_{fcs} = N_0 \left[E_{cell}^{oc\nu} + \frac{R_{gas}T}{2F} \log \left[\frac{p_{H_2}\sqrt{P_{O_2}}}{p_{H_2O}} \right] \right]$$
(9)

The FC system consumes hydrogen according to the power demand. The hydrogen required for stack operation is obtained from a high-pressure hydrogen tank. The Matlab/Simulink-based FC system model and the parameters of the PEM FC system model are shown in Fig. 3 and listed in Table 1, respectively. The PEMFC system model presented is simple and it does not account for some of the most important challenges present on PEMFC operation such as water and heat management. PEMFC stack resistance depends strongly on the level of hydration of the stack.

3.2. Dynamic modeling of battery energy system

A Nickel-Metal Hydride battery (Ni-MH battery) was modeled in reference to the R_{int} model presented in Ref. [12]. The Ni-MH battery energy system consists of four 80 Ah sub batteries in series. In general we know that I_{bat} and V_{bat} can be expressed as Eqs. (10) and (11), respectively, when the battery power consumption is *P*



Fig. 3. Dynamic model of fuel cell system.



Fig. 4. Dynamic model of battery energy system.

(12)

W. A simple dynamic model of battery energy system is shown in Fig. 4. As shown in Fig. 4 and Eqs. (12) and (13), V_{ocv} and R_{bat}^{int} are determined by using look-up tables based on experimental data presented in Fig. 5. In this paper, SOC is calculated by Eqs. (14) and (15). As shown in Eq. (15), the η in Eq. (14) is calculated depend on the battery charge/discharge status.

$$I_{bat} = \frac{V_{ocv} - \sqrt{V_{ocv}^2 - 4R_{bat}^{\text{int}}P}}{2R_{bat}^{\text{int}}}$$
(10)

$$V_{bat} = V_{ocv} - R_{bat}^{int} I_{bat}$$
(11)

where

$$V_{ocv} = f_1(SOC)$$

$$R_{bat}^{int} = \begin{cases} R_{ch} = f_2(SOC) & \text{charging} \\ R_{dis} = f_3(SOC) & \text{discharging} \end{cases}$$
(13)



Fig. 5. Characteristic of Ni-MH battery energy system.

$$SOC = SOC_{ini} - \int \frac{\eta I_{bat}}{Q} dt$$
(14)

$$\eta = \begin{cases} \eta_{ch} = \frac{V_{ocv}}{V_{ocv} - I_{bat}R_{ch}} & \text{charging} \\ \eta_{dis} = \frac{V_{ocv} - I_{bat}R_{dis}}{V_{ocv}} & \text{discharging} \end{cases}$$
(15)

4. Fuzzy logic based power management strategy

FC system efficiency can be defined as the ratio between electricity produced and hydrogen consumed, and is expressed as follows [13].

$$\eta_{FCS} = \frac{V_{c_net}}{-\Delta \bar{h}_f / 2F} = \frac{V_{c_net}}{1.482} \tag{16}$$

The mean voltage V_{c_net} can be calculated as

$$V_{c_net} = \frac{P_{fc_net}}{I_{fc}} = \frac{P_{Stack} - P_{BOP}}{I_{fc}}$$
(17)

In this paper, P_{BOP} is simply assumed to scale linearly with fuel cell output current to present the typical efficiency characteristic of fuel cell system. As a result, the net FC system efficiency is shown in Fig. 6. Therefore, the purpose of the power management strategy is to control the fuel cell power output at optimal operating conditions. The *V*–*I* characteristic of fuel cell system is shown in Fig. 7.



Fig. 6. Net fuel cell system efficiency.



Fig. 7. V-I characteristic of fuel cell system.

In order to operate the FC system efficiently, low efficient operating conditions should be avoided, as presented in Fig. 6. Therefore, under normal state of SOC, the P_{fc}^{\min} and P_{fc}^{\max} for each stack were set to 4 kW and 40 kW, respectively. However, when the SOC becomes abnormal, P_{fc}^{\min} will be set to 0 kW. The method of diagnosing abnormal SOC is described at the end of this section.

This paper makes use of a PEM fuel cell as the main power source and accordingly BES is the complementary source. The power balance of system can be expressed as

$$P_{fc} + P_{bat} = P_{load} + P_{loss} \tag{18}$$

subject to

$$P_{fc}^{\min} \le P_{fc} \le P_{fc}^{\max} \tag{19}$$

$$P_{bat}^{\min} \le P_{bat} \le P_{bat}^{\max} \tag{20}$$

where, P_{loss} is only calculated by the power converter loss of the DC/DC converter in this paper.

The fuel cell power output P_{fc} is calculated based on the SOC of battery and power demand P_{load} as follows.

$$P_{fc} = P_{fc_fuzzy} \left[1 + \frac{SOC_{ref} - SOC}{(SOC^{\max} - SOC^{\min})/2} \right]$$
(21)

where

$$P_{fc_{fuzzy}} = f(SOC, P_{load}, SOC_{diag})$$
(22)

$$SOC_{ref} = \begin{cases} 0.6 & \text{if } SOC < 0.5\\ 0.6 & \text{if } SOC > 0.7\\ SOC & \text{otherwise} \end{cases}$$
(23)

As shown in Eqs. (21), (22) and (23), fuzzy logic is utilized in the power control strategy and the design variables really being controlled are mainly P_{fc_fuzzy} and SOC_{ref} to achieve the above mentioned control goal. This paper proposes a Mamdani type's fuzzy logic controller (FLC), in which three inputs are SOC, power demand, and a diagnoses status of SOC (SOC_{diag}) and one output is $P_{fc_{-fuzzy}}$ as shown in Eq. (22). The fuzzy membership functions of the SOC, P_{load} , SOC_{diag} and $P_{fc,fuzzv}$, are shown in Fig. 8. A fuzzy rule table for $P_{fc,fuzzv}$ is Table 2. The frame of the power control procedure is shown in Fig. 9. It can be seen that to operate fuel cell system at optimal operating conditions, state machine is used in the P_{fc} identification block. That is, the three states can be explained in the following: (1) normal model: if P_{fc} determined by Eq. (21) is within allowable values, P_{fc} is not changed; (2) lower limit model: if P_{fc} determined by Eq. (21) is less than P_{fc}^{\min} , set $P_{fc} = P_{fc}^{\min}$, as a result, avoiding the fuel cell system operated at low efficient region; (3) upper limit model: if P_{fc} determined by Eq. (21) is large than P_{fc}^{max} , set $P_{fc} = P_{fc}^{max}$, thus, also avoiding the fuel cell system operated at low efficient region.



Fig. 8. Fuzzy membership function.

Table 2Fuzzy rule table for *P_{fc,fuzzy}*.

No.	Logic of judgment rules
1–3	If SOC is L & P _{load} is S & SOC _{diag} is N/VL/VH then P _{fc_fuzzy} is S/M/VS
4-6	If SOC is L & Pload is M & SOCdiag is N/VL/VH then Pfc_fuzzy is M/M/VS
7–9	If SOC is L & P _{load} is B & SOC _{diag} is N/VL/VH then P _{fc_fuzzy} is B/M/VS
10-12	If SOC is M & Pload is S & SOCdiag is N/VL/VH then Pfc-fuzzy is S/M/VS
13–15	If SOC is M & Pload is M & SOCdiag is N/VL/VH then Pfc.fuzzy is M/M/VS
16–18	If SOC is M & Pload is B & SOCdiag is N/VL/VH then Pfc_fuzzy is B/M/VS
19–21	If SOC is H & Pload is S & SOCdiag is N/VL/VH then Pfc.fuzzy is S/M/VS
22–24	If SOC is H & Pload is M & SOCdiag is N/VL/VH then Pfc.fuzzy is S/M/VS
25–27	If SOC is H & Pload is B & SOCdiag is N/VL/VH then Pfc-fuzzy is M/M/VS



Fig. 9. Frame of the power control procedure.

The foregoing functions are realized by Stateflow software in this paper.

The SOC is not always an easy value to evaluate. We deal with the error in estimating the SOC by using diagnosis table as shown in Table 3. As shown in this table, two critical states of SOC, very low and very high, are considered when SOC estimating errors are cumulated. Moreover, the states are proposed into FLC to diagnose the battery SOC as shown in Fig. 8.

Sometimes, the fuzzy control rule made in advance cannot effectively satisfy fuel cell operation requirement because of the stack aging and real-time driving cycle, etc. Therefore, this paper suggests a self-organizing method to revise the fuel cell output power based on fuzzy rule to control the SOC between 0.5 and 0.7. The procedure of deciding *SOC*_{ref} is shown in Fig. 10. It can be seen that to ensure

Table 3Diagnosis table to estimate the critical status of battery SOC.

	SOC is very high for charge model	SOC is very low for discharge model
1 2 3 4	$\begin{array}{l} 0 \leq I_{bat} \leq 1C \text{ and } V_{module} \geq 14.3V \\ 1C < I_{bat} \leq 1.5C \text{ and } V_{module} \geq 14.7V \\ 1.5C < I_{bat} \leq 2C \text{ and } V_{module} \geq 15.1V \\ I_{bat} > 2C \text{ and } V_{module} \geq 15.5V \end{array}$	$\begin{array}{l} 0 \leq I_{\text{bat}} \leq 1\text{C and } V_{\text{module}} \leq 12.3\text{V} \\ 1\text{C} < I_{\text{bat}} \leq 2\text{C and } V_{\text{module}} \leq 11.8\text{V} \\ 2\text{C} < I_{\text{bat}} \leq 3\text{C and } V_{\text{module}} \leq 11.5\text{V} \\ I_{\text{bat}} > 3\text{C and } V_{\text{module}} \leq 11\text{V} \end{array}$



Fig. 10. Logic of SOC_{ref} decision.

SOC at expected status, a state machine is also used to realize this goal by modifying SOC_{ref} .

As previously discussed, the power output of fuel cell is controlled to satisfy a slow dynamic variation which is achieved by multiplying a filter K_{filter} in the Eq. (21). The K_{filter} is used to control the DC/DC output current and determined as

$$K_{\text{filter}} = \frac{1}{1 + \tau_{\text{conv}} s} \tag{24}$$

where τ_{conv} is a time constant for DC/DC converter and it is set to 2 in this paper.

5. Simulation result and analysis

To evaluate the proposed control method, a cyclical driving simulation was conducted using the MATLAB/Simulink/Stateflow software. The SOC target value can be changed for different applications, and in the simulation, the range of between 0.5 and 0.7 was selected. A cycle driving load mode was assumed as shown in Fig. 11. The maximum load power was about 60 kW. The *SOC^{max}* and *SOC^{min}* were assumed to be 0.8 and 0.2, respectively. The simulation results are presented as follows.

Fig. 12 shows the power profile for the initial SOC of 0.7. As shown in Fig. 12, the battery discharges rapidly to react to the fast load changes and to supply the supplementary power, because the output power change of the FC stack is intentionally restricted to a slow dynamic response in order to extend the lifetime of the FC system. Meanwhile, the FC power is used dynamically to charge the battery, thus maintaining the SOC target value when the load power is lower or zero. Fig. 13 shows the distribution percentage for the fuel cell output power. It is illustrated that the fuel cell system is operated at high efficiency scopes.



Fig. 11. Load profile for single-cycle simulation.



Fig. 12. Power profile for initial SOC of 0.7.



Fig. 13. Distribution percentage of fuel cell output power.

Fig. 14 shows the power profile for the initial SOC of 0.7. In Fig. 14, it is evident that, using the proposed control methodology, the SOC of the battery energy system can be maintained around the target range. Meanwhile, the battery voltage is changed as shown in Fig. 15.

Fig. 16 shows the change of SOC considering different initial SOC of battery energy system. It is obtained from a case of setting a target SOC of 0.7 during the cycle's driving simulation. From this figure, it is apparent that the SOC of the battery can be effectively maintained around the target value of 0.7 by using the proposed



Fig. 14. SOC profile for initial SOC of 0.7.



Fig. 15. Battery voltage profile for initial SOC of 0.7.



Fig. 16. Change of SOC according to different initial SOC.

fuzzy modification concept to flexibly adjust the fuzzy logic based FC power output.

6. Validation and analysis

To evaluate the performance of the proposed power control strategy, some road driving tests were conducted using fuel cell hybrid vehicle (FCHV) shown in Fig. 17. The FCHV began operating as part of a 1-year-long Olympic demonstration in Beijing [14]. The specifications of the FCHV are shown in Table 4. Fig. 18



Fig. 17. Fuel cell hybrid vehicle.

Table 4

Specifications of FCHV in Beijing.

1	Fuel cell system	
	Type Output voltage Cooling mode	PEM 360–520 V Water
2	Hydrogen Type Rated hydrogen vessel pressure	Pure 20 Mpa
3	DC/DC converter Type Input voltage Output voltage Cooling mode	Buck 360–520 V 300–420 V Water
4	Battery system Type Nominal voltage Capacity No. of modules	Nickel-Metal Hydride 336 V 80 Ah 28
5	Motor Type Rated power Maximum output power Maximum output torque Maximum rotate speed Cooling mode	Induction 100 kW 185 kW 1100 Nm 6000 rpm Water



Fig. 18. Vehicle speed profile during road test driving period.

shows vehicle speed profile during 2400 s road test driving period. Figs. 19 and 20 show the test results for the FCHV, where the power train was controlled by the proposed power management strategy using fuzzy logic. From Figs. 19 and 20, it can be seen that the SOC



Fig. 19. Test result of power profile for FCHV.



Fig. 20. Test result of SOC profile for FCHV.

of battery can be maintained around the target conditions through real-time power flow control.

7. Conclusions

In this paper, a fuzzy logic based power management strategy that secures the power balance and maintains the SOC in a hybrid FC vehicular power system is proposed. Simulation results and road driving tests demonstrate that the proposed method can control the FC system within a specified high-efficiency region and manage the system power flows to maintain the SOC of the battery around the target conditions. The optimal power control including hydrogen utilization will be discussed in the near future with a regenerative braking control of fuel cell hybrid vehicle.

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